## CO<sub>2</sub>Capture Project



CO<sub>2</sub> Capture Project

#### **BUILDING ON CCP1 RESULTS**





CCP1 favored technologies achieved:

## ✓ Proof-of-Feasibility

- Concept successfully tested at the lab scale
- Critical items for development identified.
- Potential for consistent reduction in CO<sub>2</sub>
  Capture costs compared to currently available technology.















### **CCP** Scenarios

Scenario		CO <sub>2</sub> -generating fuel	Uncontrolled CO <sub>2</sub> -emission
UK Refinery	Heaters & Boilers in existing refinery	Refinery fuel oil and gas	2,6 mill.ton/yr from target H&B's
Alaska Turbines	Small powergen turbines in operation	Natural gas	2,6 mill.ton/yr
Norway Gas Power	New 400 MW CCGT-plant	Natural gas	1,3 mill.ton/yr
Canada coke gasifier	New IGCC-plant	Petroleum coke	4,9 mill.ton/yr









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#### CCP2 Technology Portfolio Main Features

- Technologies with different "time to market" in a sequenced approach:
  - Short Term (by 2010)
  - Mid-Term (2010-2012)
  - Long Term (by 2015)
- Emphasis on Pre-Combustion technology, but continuation of most promising Post-Combustion and Oxy-firing Projects.







#### CCP2 Capture Program Targets

- Achieve significant progress for each technology:
  - Scaling-up successfully operation by at least one order of magnitude.
  - Addressing and solving critical issues identified in CCP1

 At least one technology ready for field demonstration by the end of the Project.







#### CCP2 Capture Program Timeline

#### **2004**

- Selection of Technology Portfolio.
- Preparation of Project Proposals.
- Submission to Governmental funding entities (Oct-Dec).
- **2005**
- Approval of Project Proposals (Mar-May).
- Definition of further needs
- Start Technical Program (Sep-Dec).
- Prepare additional proposal if necessary.
- **2006-2008**
- Run technical Program to completion maintaining stage gate approach.
- Update economical evaluations.
- Continue monitoring of novel concepts and competing technologies.







### The CCP2 Portfolio (Jan. 2006)

- Pre-Combustion
  - CO2 separation technologies
    - Membrane Water Gas Shift (MWGS)
    - Sorption Enhanced Water Gas Shift (SEWGS)
  - Novel Syngas/Hydrogen production technologies
    - Hydrogen Membrane Reforming (HMR)
    - Chemical Looping Reforming
    - One-Step Hydrogen
    - HyGenSys
    - Membrane Reforming

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## The CCP2 Portfolio (Jan. 2006)

- Post-Combustion
  - BIT (Best Integrated Technology)
- ❑ Oxy-firing
  - Chemical Looping Combustion (CLC)







## The CCP2 Projects

- □ Three major Projects approved:
  - CLIMIT (Co-Funder Norwegian Council for Research)
  - CACHET (Co-Funder European Union)
  - CLCGASPOWER (Co-funder European Union)







# CO<sub>2</sub> Capture Project

## CLIMIT

- Co-Funder: Norwegian Council for Research)
- Duration: 36 Months (started September, 2005)
- Total Budget: ~ 7 MM\$ (subject to exchange rate)
  ~ 90% Capture
- > Technologies Included:
  - oHMR(Hydro): 36 MonthsoMWGS(Sintef): 6 Months
  - o BIT (GE) : 8 Months









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#### **Hydrogen Membrane Reformer: The Concept**

- •Combination of reforming reactor and separation
- •Extract product gas (H<sub>2</sub>) from reactor, no traditional CO<sub>2</sub> removal system required
- •Drive equilibrium limited reactions towards completion
- •Expand allowed range of temperatures and pressures







#### Hydrogen Membrane Reforming

- Strategic Features
  - Long Time to Market (2015)
  - > High Potential for Cost Reduction (< 30 \$/ton CO2 avoided)</p>
  - > Application to Power Generation from Natural Gas
- CCP1 Achievements
  - > Developed materials with good permeability and stability
  - Developed method for manufacturing supproted membranes in the form of small tubes (10cm length, overall diameter 8mm).









#### Hydrogen Membrane Reforming

#### CCP2 Expected Development

- > Develop membranes in the form of monoliths.
- Successfully test at the laboratory level 2X2 cm monoliths.
- Fabricate 7x7 cm monoliths that will form the base unit for pilot plant (25 kW).
- Review and optimize process scheme including collaboration with turbine vendor.







## CO<sub>2</sub> Capture Project

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#### **Best Integrated Post-Combustion Technology**





#### **Best Integrated Post-Combustion Technology**

#### Strategic Features

- Short Time to Market (2008-2010)
- > High Potential for Cost Reduction (< 30\$/ton CO2 avoided)</p>
- > Application to Power Generation from Natural Gas

#### CCP1 Achievements

Developed low-cost integrated process scheme based on application of concepts developed in engineering study.







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#### **Best Integrated Post-Combustion Technology**

#### CCP2 Expected Development

- Assess feasibility and constraints of flue gas recycle to combustor.
- > Evaluate use of novel solvents.
- Review and further optimize the CCP1 process scheme.
- Include novel concepts under development.







## CLCGASPOWER

- **Co-Funder:** European Union
- Type of Project: STREP
- Duration: 30 Months (Started January 1st, 2006)
- AAAA Total Budget: ~ 2.8 MM\$ (subject to exchange rate)
- Single Technology Development of Chemical Looping Combustion by a Consortium formed by:
  - **Chalmers University of Technology** 0
  - **Alstom Boilers** 0
  - **CSIC** 0
  - Shell 0
  - Vienna University of Technology 0
  - **Tallinn University of Technology** 0





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# CO<sub>2</sub> Capture Project

#### **Chemical Looping Combustion**

- Chemical Looping is a new combustion technology based on oxygen transfer from combustion air to the fuel by means of a metal oxide acting as a solid carrier. Core of the technology is a two-reactors system with continuous circulation of solids:
- Fuel reactor:  $4MeO + CH_4 \Rightarrow 4Me + 2H_2O + CO_2$
- Air reactor:  $4Me + 2O_2 \Rightarrow 4MeO$













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## **Chemical Looping Combustion**

#### Strategic Features

- Mid Time to Market (2010-2012)
- > High Potential for Cost Reduction
- > Application to gas fired boilers/ steam turbine power generation

#### **CCP1 Achievements**

- Developed materials with good activity by extensive screening and development.
- Achieved proof-of feasibility in a 10kW bench scale unit with continuous solid circulation.





## **Chemical Looping Combustion**

#### CCP2 Expected Development

- Assess long time resistance (both chemical and mechanical of developed materials)
- Scale-up to 200kW pilot unit c/o Vienna University of Technology.
- > Prepare concept design for demo unit (20-50 MW).





## CO<sub>2</sub> Capture Project

## CACHET

- > Co-Funder: European Union
- Type of Project: Integrated Project for Production of Hydrogen from Natural Gas with CO<sub>2</sub> Capture
- > Duration: 36 Months (starting March 1st, 2006)
- > Total Budget: ~ 16.5 MM\$ (subject to exchange rate)
- Consortium of 29 Partners from 18 Countries.
- > Targets:
  - Develop in parallel to "ready-for-pilot" several novel
    hydrogen production and pre-combustion CO<sub>2</sub> Capture Technologies.
  - Identify optimal process scheme through optimized integration of technologies driven by economic evaluation.









## **Membrane Water Gas Shift**





## **Membrane Water Gas Shift**

#### Strategic Features

- Mid Time to Market (2010-2012)
- Mid Potential for Cost Reduction
- Preferential application to heaters/boilers or steam turbine power generation from natural gas.

#### **CCP1 Achievements**

- Developed very thin palladium layers (< 5µ) supported on porius stainless steel (SINTEF)
- Developed vanadium membranes in palladium layers sandwich to improve permeability (Eltron).

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## **Membrane Water Gas Shift**

#### CCP2/CACHET Expected Development (SINTEF/ECN)

- Develop and test supported palladiu membranes in the form of 1 meter long tubes (I.D. 12.5 mm)
- Build and operate a bench scale reactor module (12 tubes) with hydrogen production roughly equivalent to 15-30 kW.









## Sorbent Enhanced Water Gas Shift



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## **Sorbent Enhanced Water Gas Shift**

#### Strategic Features

- Short Time to Market (by 2010)
- Mid/High Potential for Cost Reduction
- Preferential application to power generation from natural gas in combined cycle.

#### CCP1 Achievements (Air Products)

- > Develop modified hydrotalcites with good adsorption properties.
- Successfully tested in a single lab reactor with alternate adsorption/desorption.







## **Sorbent Enhanced Water Gas Shift**

CCP2 Expected Development (Air Products/ECN)

- Further optimization of adsorbent materials.
- Build and operate a lab unit with 7 reactors in parallel to simulate the commercial operating cycle. Reactors with full commercial length and small diameter.









## **Chemical Looping Reforming**







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## **Chemical Looping Reforming**

- Mid/Long Term time to market (2012/2015)
- CCP2 Expected Development (CLC Consortium)
  - Screening and optimization of solid carrier materials at the lab scale.
  - Engineering development will benefit from parallel CLC development.











## **One-Step Hydrogen**





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## **One Step Hydrogen**

- Long Term time to market (~ 2015)
- CCP2 Expected Development (EniTecnologie)
  - > Optimization of solid carrier materials at the lab scale, and scaleup of production with commercial manufacturer.
  - Reactor and Process scheme optimization
  - > Hydrodynamic optimization through "mock-up" with continuous solid circulation.









## HyGenSys

HyGenSys is a novel reforming technology based on the Gas Heating concept (avoidance of furnace emissions) and strict integration with a gas turbine. In the power generation mode, hydrogen burning in the turbine is needed for zero emission.









## HyGenSys

- Short Term time to market (by 2010)
- CCP2 Expected Development (IFP)
  - > Process Optimization with turbine vendor.
  - Reactor mechanical design.
  - > Hydrodynamic optimization through large "mock-up"









## Low Temperature Membrane Reforming

Novel reforming technology based on the development of dense Pd alloy membranes to separate hydrogen as it is formed, able to operate at a temperature of about 600°C.









## Low Temperature Membrane Reforming

- **Long Term time to market (by 2015)**
- CCP2 Expected Development (ECN, SINTEF)
  - > Development of suitable membranes at laboratory level.
  - > Test in base module reactor (the same designed for MWGS).









#### Completion of CCP2 Portfolio Coal Gasification

- CCP1 showed that, once the coal gasification route is selected, additional cost for CO<sub>2</sub> Capture is very low.
- Cryogenic technology seems to be favoured due to potential poisoning of any catalyst, solvent or sorbent.
- The Capture Team is finalising CCP2 work programme in this field.











## The CCP2 Time Sequenced Portfolio

- Short Term (~ 2010)
  - 。SEWGS
  - 。BIT
  - 。HyGenSys
- Mid-Term (~ 2012)
  - o Chemical Looping Technologies
  - MWGS
- Long Term (~ 2015)
  - 。HMR
  - o One-Step Hydrogen
  - Low Temperature Membrane Reforming.

